

EXHIBIT A



**SeangYong Oil Refining Co., Ltd.**

360 SANAM-RI, ONSAN-MYUN ULSAN-KUN, KYUNG NAM 688-080, KOREA

Phone : 82-522-31-2350

Fax : 82-522-39-0118

PACIFIC/ASIA DIVIS.

## FACSIMILE TRANSMISSION

Date : [REDACTED]

Fax number : 1-214-583-3055

To : Mr. Kuang Wu, Marketing Manager Pacific/Asia Div.

CC : Adam T. Lee, Glitsch Co.

고 석환 이사, 영광상사

From : H. J Chae, BTX Production Dept. Manager

Number of pages : 4 pages(including this sheet)

Message : Questionnaire about Tower Modification

Dear Mr. Kuang Wu,

It is my pleasure to contact with you. I'm a manager of BTX production department in SSangYong Oil Company, Korea. I heard that you had had connection with engineering department of my plant, referred to installation of Bz recovery column. Since I have constructed the #2 Sulfolane Unit, the Bz recovery Project was cancelled. I'm sorry that such connection should have come to such a pass.

By the way, I need to replace the tower tray, because I have to increase the Reformate Splitter(T-7501) Charge. Thus, I want feasibility survey about to increase the Charge with tray replacement. I attach the data referred to Process Scheme(1) and Stream Data(Design, Actual & Target composition))(2).

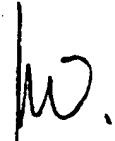
I look for your reply in that following questions.

- 1) If the trays are replaced with highperformance type(I want the best quality), will it be possible to operate 40,000 BPD?
- 2) If it is impossible, what will be the Max. charge rate in both cases(actual tray, highperformance tray)?
- 3) Additionally, what are the required Heat duties(O/H Condenser, Reboiling Heater) in both cases?
- 4) I can't modify the Reboiling heater(H-7501) and O/H condenser, so I consider new preheater installation in feed stream. If I install the preheater, how much will the required heat duty decrease, moreover what about the O/H condenser Duty ?

- 5) How much do I need a total replace cost?
- 6) How much do you need a time of engineering, produce, and delivery? we have to replace the tray during the '96 total turn-around period(June '96).

Best Regards,

Sincerely yours,



H. J. Chae

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